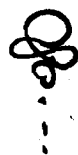


*The Heat of Adsorption of Oxygen
on Charcoal.*

by
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A Thesis submitted for the Degree of

MASTER OF APPLIED SCIENCE

in the Department of

CHEMISTRY

THE UNIVERSITY OF BRITISH COLUMBIA

April, 1925.

Approved E.H.C.

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THE HEAT OF ADSORPTION OF OXYGEN ON CHARCOAL.

Introduction

The first quantitative work on the adsorption of gases on charcoal was carried out by de Saussure¹. Since that time many investigations have been prosecuted to determine the quantitative relationships existing between quantity of gas adsorbed, temperature and pressure. In a few cases (Favre², Chappins³, Titoff⁴, Lamb and Coolidge⁵, Blench and Gainer⁶,) the heat of adsorption has been measured at different temperatures and pressures. Dr. M.J. Marshall⁷, while working on the heats of adsorption of gases and vapours on charcoal, obtained very striking results in the case of low concentration of oxygen. He found:

1. that the initial heat values were very high - 70000 cal./mole/ gm. of charcoal, and the final values very low - 4000 cal./ mole/ gm.
2. the first adsorption was characterized by the satisfaction of primary valences, further adsorption resulting from a modification of existing molecular fields.
3. the active surface of the charcoal was very small, approximately 0.5 sq. metres per gm. He used only a small quantity of charcoal- 2 to 3 gms., and his ice calorimeter could only be relied upon for five hours. Further, the charcoal used was French war charcoal, very likely not the most active available. The present research was instituted in order that the previous conclusions might be checked with a different type of charcoal, using a larger quantity to enable a closer study of the initial heats to be made, and working under calorimetric conditions permitting a more leisurely study of the heat evolution.

GENERAL EXPERIMENTAL PROCEDURE.

1. Preparation of Charcoal

The charcoal used was a standard sample of activated cocoanut charcoal obtained from the National Carbon Co. Before use it was extracted repeatedly with hydrochloric acid to remove any soluble salts, and then with hydrofluoric acid to remove the silica. This reduced the ash content to 0.2668%. Finally it was graded to pass a mesh of cross-sectional area 2.725 sq. mm. and be retained on one 0.689 sq. mm. Prior to the first run the charcoal was exhausted at 1000° C. for sixty hours. The final pressure was 1×10^{-4} cm. at this temperature. The pumps were kept going until the mass had cooled to room temperature. The exhaustion preparatory to the second run required only ten hours pumping at 1000° C.

2. Preparation of Oxygen

The oxygen was prepared by gently heating anhydrous potassium chlorate containing a trace of manganese dioxide. In a previous run no manganese dioxide was used and a severe explosion occurred.

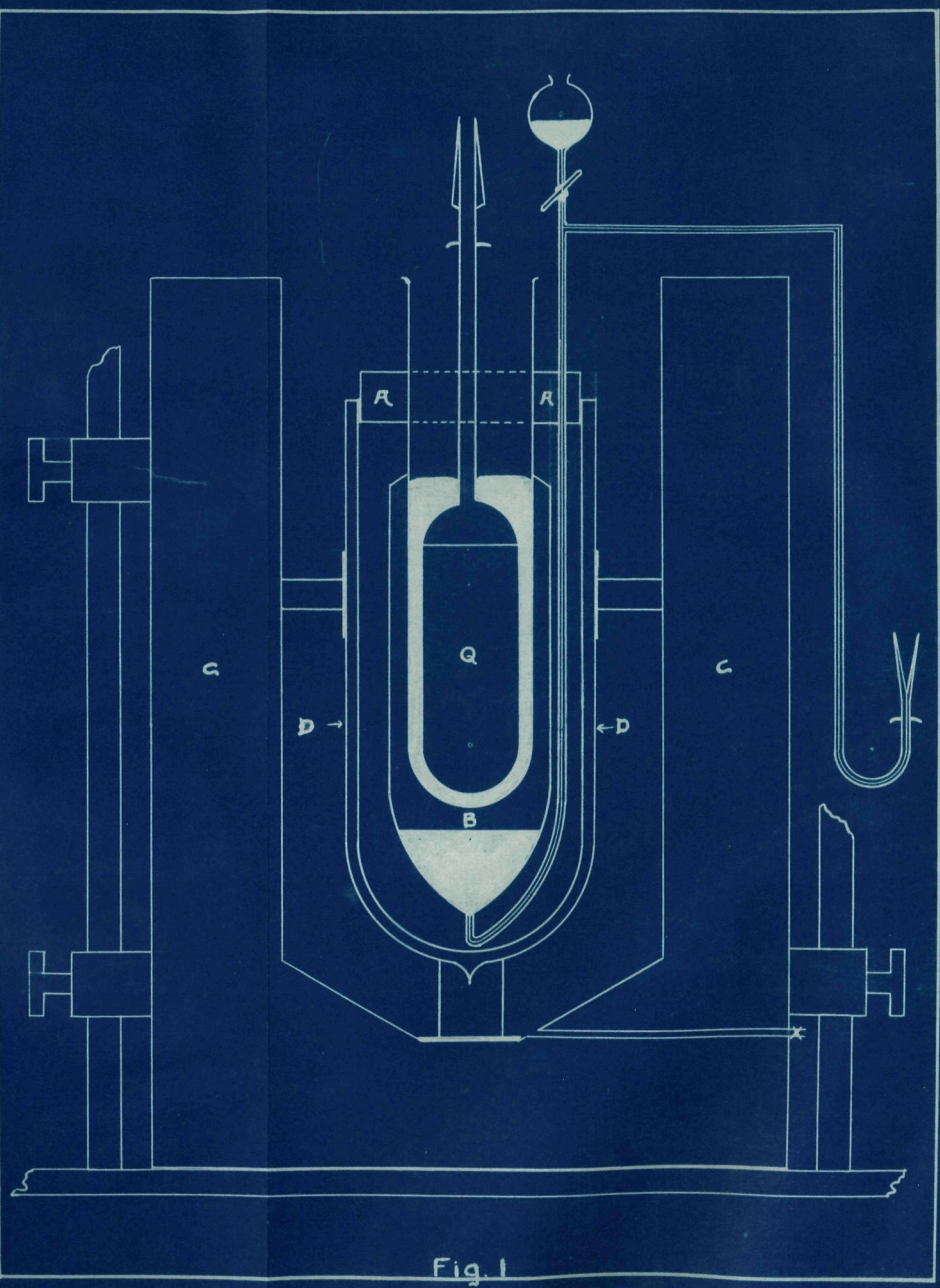
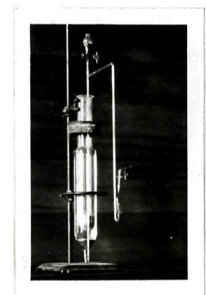
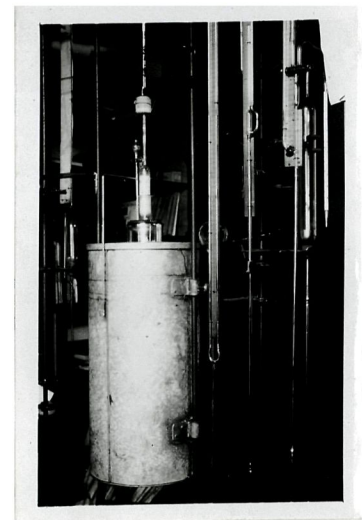
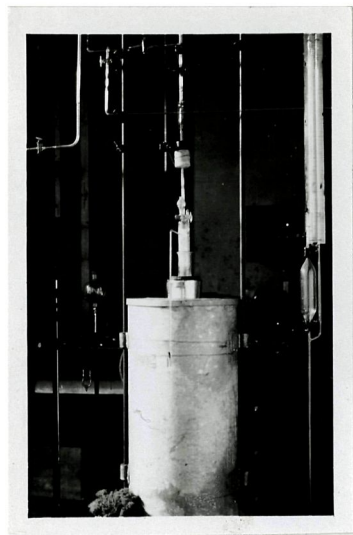


Fig. 1



3. Apparatus

The apparatus used is shown in the accompanying diagram and photographs. The feature of the apparatus is the calorimeter, a modification of that designed by Griffiths⁸. It consisted of the galvanized iron container C, the jacket of which was packed with felt; the Dewar flask D, and the Bunsen ice calorimeter B. The cork A provided a water-tight seal when the ice calorimeter was lowered into the Dewar flask and this permitted crushed ice to be packed in C up to the top of B. A plug of felt was packed around the quartz tube where it entered the neck of B. Distilled water was added up to the ice level. Using this arrangement an ice mantle was maintained in B continuously for twenty days.

The charcoal was contained in the quartz bulb Q. This bulb was lined with platinum in order to prevent the reduction of the quartz by the carbon at the high temperatures of evacuation.

Contact between the walls of the ice calorimeter and the bulb Q was made by means of a film of mercury.

A very even ice mantle inside the Bunsen calorimeter was obtained by immersing a long tube containing an ether-solid carbon dioxide mixture in the mercury. This tube was slightly larger than Q. By adjusting the level of the mercury a mantle of uniform thickness was obtained.

The performance of the calorimeter was studied for eight days. As a result it was found possible to maintain a constant leak for periods of sixteen - eighteen hours. The absolute value of the leak could be varied by adjusting the room temperature. As a result of studies made during the first run it was determined that the value of the leak increased with additions of gas, the increment from run to run being very small. Values of the leak varying from zero to .03 cm. per five minutes were obtained. The crushed ice had to be renewed every twenty-four hours when the room was kept at 20° C.

4. Method

The quartz bulb Q was charged with about 25 gms. of charcoal, exhausted at 1000° C. for several hours, filled with hydrogen, sealed and weighed. The charcoal was again exhausted as described above. When this was complete the ice calorimeter was prepared and the apparatus assembled for a run. The whole was given two days to stabilize in before a run was commenced. At first small quantities, less than 1 c.c., of oxygen were admitted to the charcoal. These were increased until about 70 c.c. quantities were admitted. The heat evolved was measured by means of the drop in mercury in the capillary tube. This tube was carefully calibrated on the basis of one mean calorie equal to 0.01549 grams of mercury⁸. A single charge was

studied for a period of from nine to twenty hours.

RESULTS.

Two runs were made. The data are shown in Tables I and II. The total calories per gram of charcoal, q , was plotted against total moles $\times 10^4$ of oxygen adsorbed per gram of charcoal, n , on a very large scale. This curve is reproduced in Fig. 2. The tangents to this curve, $\frac{dq}{dn}$, will give the values of the heat of adsorption at constant volume per gram molecule of gas per gram of charcoal, Q_v , at the concentration n . These values are given in Table III and plotted in Figure 3.

After completion of run B the apparatus was maintained at 0°C . while the gas was pumped off by means of a Topley pump. The gas was passed through baryta water. Only a very slight precipitate was formed.

While conducting the preliminary exhaustion to run A, it was noticed that after prolonged exhaustion at 1000°C the charcoal and quartz bulb were charged electrostatically with charges of opposite sign. If a piece of charcoal came in contact with the quartz it would adhere. By sharply tapping the bulb the charcoal could lie detached and it would then pass in a curved orbit to a new point on the quartz, maintaining the same general level. After being detached several times it would fall back into the mass of charcoal.

DISCUSSION OF RESULTS.

Examination of Figure 3 shows that the initial heat of adsorption is very high, 84,400 calories per mole per gram. This value is higher than any previous value the highest recorded being 70,000 calories per mole per gram due to Marshall. The final values are the same in each case - approximately 4000 calories per mole per gram.

In view of the high initial values it would seem that the first quantities adsorbed were held by primary valences, later layers being held by modification of the existing molecular fields. The curve in Figure 3 is also periodic in nature, tending to have steps occur at increasing concentration intervals. This periodicity gives an explanation of the phenomenon observed:

During the preparation of charcoal the carbon chains existing in the fibres are denuded of their hydrogen but are not much modified, if at all, in form. The result is that a certain few atoms will be thrust clear of the aggregate and present a point of intense attraction for the oxygen. Also, although the charcoal has a general porosity, it also contains some pores of molecular dimensions in the carbon chains. These pores will also represent regions of intense attraction. Since the attractive forces at these points will of necessity be very variable no constant heat value could be expected until they are all

covered with at least a monomolecular layer. Even then prominent points would have greater attractive properties than the general surface and hence would still tend to attract the oxygen preferentially. A constant heat value would not be obtained until they were saturated, or rather their attractive force reduced to a value represented by the attractive force of the general surface. Then a general covering would occur, after which the heat value would be a more or less constant low value. The point representing a monomolecular layer would be the concentration at which the heat values drop off to approximately a constant value. Hence, assuming that the first layer corresponds to 1×10^{-4} grams molecules of oxygen, that $N = 6.06 \times 10^{23}$, and that the distance apart of the centres of the oxygen atoms is 1.25×10^{-8} cms. as shown by Bragg⁹, we can calculate the minimum surface per gram of charcoal as follows:

$$\begin{aligned} S &= 2 \times 1 \times 10^{-4} \times 6.06 \times 10^{23} (1.25 \times 10^{-8})^2 \\ &= 1.8937 \times 10^4 \text{ sq. cm. per gm.} \\ &= 18.937 \text{ sq. metres per gm.} \end{aligned}$$

SUMMARY

1. The heat of adsorption of oxygen on charcoal at 0° C. has been carefully measured over a large range of concentrations, using 25 grams of cocoanut charcoal.
2. The initial concentrations used are smaller, and the initial heats larger than those obtained by any previous investigator.
3. The mechanism of adsorption has been discussed.
4. The active surface of cocoanut charcoal has been calculated to be 18.937 sq. metres per gm.
5. Charcoal has been heated for sixty hours at 1000° C. without apparent loss of activity, although previous investigators claimed great loss of activity from continued heating above 800° - 900° C.
6. The activity of charcoal depends more upon the temperature of evacuation than upon the time.
7. No appreciable quantity of carbon dioxide is formed when oxygen is adsorbed at 0° C.
8. Interesting electrical phenomena have been observed after long heating and continued evacuation.

Further work is being done in connection with the oxygen results. It is hoped to measure the heat of adsorption of acetylene.

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TABLE I.

		Wt. of Charcoal = 25.7920 gr.							
Run	gas Admitted	Final Pressure mm.	Total gas not adsorbed	Gas adsorbed	Total c.c. adsorbed	Heat in Cal...	Total Heat	q = cal 1 gm.	R x 10 ⁴ = Moles 1 gm.
A 1	0.8728	0.0	0	0.8728	0.8728	3.203	3.203	.1242	.015115
2	1.2120	0.0	0	1.2120	2.0848	3.828	7.031	.2715	.036103
3	2.4951	0.0	0	2.4951	4.5799	7.371	14.402	.5584	.079307
4	0.8466	0.0	0	0.8466	5.4265	2.350	16.752	.6495	.096694
5	1.1904	0.0	0	1.1904	6.6169	3.008	19.760	.7661	.114580
6	2.0984	0.0	0	2.0984	8.7153	6.253	26.013	1.0087	.150940
7	2.4501	0.0	0	2.4501	11.1654	7.162	33.175	1.2862	.193340
8	2.2044	0.0	0	2.2044	13.3698	6.602	39.777	1.5422	.231540
9	3.2036	0.0	0	3.2036	16.5734	9.344	49.121	1.9046	.287000
10	2.2572	0.20	.0237	2.2335	18.8069	7.637	56.758	2.2006	.325700
11	3.5713	0.34	.0403	3.5547	22.3616	6.910	63.668	2.4684	.404270
12	6.8989	3.25	.3860	6.5532	28.9148	11.453	75.121	2.9127	.500720
13	6.8562	7.40	.8832	6.3590	35.2738	8.631	83.752	3.2472	.610800
14	10.5830	14.73	1.7741	9.6921	44.9659	8.253	92.005	3.5672	.778700
15	22.3205	35.60	4.2861	19.8085	64.7744	6.854	98.859	3.8330	1.121730
16	29.4030	83.40	9.5605	24.1286	88.9030	7.036	105.895	4.0954	1.532400
17	45.7284	140.00	16.7946	38.4943	127.3973	8.127	114.022	4.4207	2.206300
18	27.9632	179.20	21.6260	23.1318	150.5291	4.476	118.498	4.5945	2.605550
19	62.3590	271.50	33.1900	50.7950	201.3241	10.434	128.932	4.9990	3.48780
20	77.0983	382.20	46.4470	63.8413	265.1654	11.260	140.192	5.4356	4.59920

TABLE II.

Wt. of Charcoal = 24.8428 gms.

Run	Gas Admitted	Final Pressure (mm)	Total gas not adsorbed	Gas adsorbed	Total c.c. gas adsorbed	Heat in Cal.	Total Heat in Cal.	q = Cal/ gm.	R x 10 ⁴ Moles/ gm.
B 1	.7572	0	0	.7572	.7572	2.966	2.966	0.1194	.013614
2	1.4952	0	0	1.4952	2.2524	5.091	8.057	0.3243	.040493
3	2.4695	0	0	2.4695	4.7229	8.015	16.072	0.6469	.084910
4	3.7552	0	0	3.7552	8.4781	11.274	27.346	1.0951	.152420
5	3.8696	.05	.0060	3.8636	12.3417	11.792	39.138	1.5754	.221905
6	7.4069	.40	.0479	7.3650	19.7067	20.702	59.840	2.4091	.354300
7	11.3680	6.85	.8202	10.5957	30.3024	14.910	74.750	3.0091	.544775
8	15.5690	20.25	2.4242	13.9650	44.2674	11.246	93.102	3.6091	.795772
9	20.4246	43.50	5.2123	17.6365	61.9039	5.945	99.047	3.8402	1.113000
10	67.9940	128.20	15.3671	57.8382	119.7421	15.290	115.337	4.4715	2.153000
11	87.5640	259.0	31.0660	72.8651	192.6072	15.848	130.820	5.0715	3.462600
12	73.2420	374.0	44.9310	59.3770	251.9842	11.583	142.403	5.5211	4.530000
13	75.2550	513.9	61.4760	58.7100	310.6942	11.400	153.803	5.9631	5.58580

TABLE III.

$N \times 10^4$	$\frac{dg}{dn}$
0	85,200
0.01	84,400
.02	81,100
.05	73,970
.10	69,800
.15	68,263
.20	63,165
.30	59,000
.40	42,667
.50	32,500
.60	28,400
.70	19,467
.80	12,217
1.00	7,266
1.50	5,900
2.00	5,166
2.50	4,633
3.5 - 6.0	4,250

